

 برکت پالایش نفت بندرعباس BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668		BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER		PHASE: EB								
MC:HEIDCO 		 Research Institute of Petroleum Industry		HEAT AND MATERIAL BALANCE FOR SWS UNIT		SPEC. NO: 108-GP-E-411833		UNIT/ITM: 108				
						REV.	0	1	2	B0		

DOCUMENT TITLE:

HEAT AND MATERIAL BALANCE
FOR
SWS UNIT

DOCUMENT NO: 108-GP-E-411833

TOTAL PAGES: 8

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2	2021.JUN.28	For Approval	IFA		ARY	AAD	BGO
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 شرکت پالایش نفت بندرعباس BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668		BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER				PHASE: EB								
MC:HEIDCO		 Research Institute of Petroleum Industry		HEAT AND MATERIAL BALANCE FOR SWS UNIT				PROJ. NO.1668		UNIT/ITM: 108				
 HEIDCO								SPEC. NO: 108-GP-E-411833		SH/OF: 1 / 8				
								REV.	0	1	2	B0		

Sheet No.	Internal Issue	CHANGE INDEX DURING FORMAL ISSUES					Sheet No.	Internal Issue	CHANGE INDEX DURING FORMAL ISSUES				
		First Issue	Second Issue	Third Issue	Fourth Issue			First Issue	Second Issue	Third Issue	Fourth Issue		
NO.	REV. A	REV.0	REV.1	REV.2	REV.B0		NO.	REV. A	REV.0	REV.1	REV.2	REV.B0	
1		√	√	√	√		51						
2		√	√	√			52						
3		√	√	√			53						
4		√	√	√			54						
5		√	√	√			55						
6		√	√	√			56						
7		√	√	√			57						
8		√	√	√			58						
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 شرکت پالایش نفت بندرعباس BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668			BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER						PHASE: EB							
									PROJ. NO.1668			UNIT/ITM: 108				
MC:HEIDCO		 Research Institute of Petroleum Industry		HEAT AND MATERIAL BALANCE FOR SWS UNIT						SPEC. NO: 108-GP-E-411833			SH/OF: 2 / 8			
				REV.		0		1		2		B0				
1	Stream Number			01		02		03		04		05				
2	Stream Name			SOUR WATER TO SURGE DRUM		OFF GAS FROM SURGE DRUM		RECOVERED OIL TO PUMP (Note 1)		RECOVERED OIL TO SLOPS TANK (Note 1)		SOUR WATER FROM SURGE DRUM				
3																
4	Stream Description		Unit													
5	Vapor Mass Percent		wt%		0.01		100.00		0.00		0.00		0.00			
6	Temperature		°C		54		53		54		54		54			
7	Pressure		bar (g)		2.2		1.1		(Note 3)		5.4		(Note 3)			
8	Total Mass Flow		kg/h		99264.7		17.3		(Note 1)		113.8		99133.7			
9	Total Mol Flow		kmol/h		5458.4		0.6		(Note 1)		1.4		5456.4			
10	Total Heat Flow		MW		-423.71		0.0		(Note 1)		-0.1		-423.63			
11	Total Molecular Weight		kg/kmol		18.19		29.64		81.77		81.77		18.17			
12	Total Flowing Density		kg/m³		917.4		2.3		632.6		632.9		955.8			
13																
14	Liquid Phase															
15	Mass Flow Rate		kg/h		99250.3				(Note 1)		113.8		99133.7			
16	Molar Flow Rate		kmol/h		5457.9				(Note 1)		1.4		5456.4			
17	Flow Rate @ op. cond.		m³/h		103.9				(Note 1)		0.2		103.7			
18	Standard Volume Flow Rate		m³/h		102.6				(Note 1)		0.2		102.5			
19	Molecular Weight		kg/kmol		18.18				81.77		81.77		18.17			
20	Flowing Density		kg/m³		955.3				632.6		632.9		955.8			
21	Specific Gravity @ 15/15 °C		-		0.9679				0.6675		0.6675		0.9685			
22	Viscosity		cP		0.4602				0.2265		0.2260		0.4590			
23	Surface Tension		dyne/cm		46.05				14.96		14.93		45.95			
24	Mass Enthalpy		kJ/kg		-15368.7				-2331.4		-2330.5		-15384.1			
25	Mass Heat Capacity		kJ/(kg.°C)		3.9505				2.3445		2.3440		3.9524			
26	Thermal Conductivity		W/(m.K)		0.6123				0.1096		0.1095		0.6138			
27																
28	Vapor Phase															
29	Mass Flow Rate		kg/h		14.5		17.3									
30	Molar Flow Rate		kmol/h		0.5		0.6									
31	Flow Rate @ op. cond.		m³/h		4.3		7.4									
32	Molecular Weight		kg/kmol		28.06		29.64									
33	Flowing Density		kg/m³		3.3616		2.3319									
34	Viscosity		cP		0.0115		0.0114									
35	Compressibility Factor		-		0.9862		0.9896									
36	CP/Cv Ratio		-		1.1887		1.1798									
37	Mass Enthalpy		kJ/kg		-1733.1		-1744.2									
38	Mass Heat Capacity		kJ/(kg.°C)		1.9805		1.9224									
39	Thermal Conductivity		W/(m.K)		0.0533		0.0496									
40																
41	Stream Composition				mol %	wt %	mol %	wt %	mol %	wt %	mol %	wt %				
42	N2				0.00	0.00	0.89	0.84	0.00	0.00	0.00	0.00	0.00	0.00		
43	H2				0.01	0.00	44.33	3.01	0.10	0.00	0.10	0.00	0.00	0.00		
44	C2				0.00	0.00	0.59	0.60	0.04	0.01	0.04	0.01	0.00	0.00		
45	C3				0.00	0.00	0.42	0.63	0.08	0.04	0.08	0.04	0.00	0.00		
46	C4				0.00	0.00	0.32	0.62	0.17	0.12	0.17	0.12	0.00	0.00		
47	C5+				0.03	0.14	20.26	58.91	92.76	97.75	92.76	97.75	0.00	0.02		
48	CO2				0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
49	H2S				1.00	1.87	28.07	32.27	2.82	1.18	2.82	1.18	0.99	1.87		
50	NH3				0.96	0.90	0.08	0.05	0.01	0.00	0.01	0.00	0.96	0.90		
3	Water				98.01	97.09	5.04	3.06	4.02	0.88	4.02	0.88	98.04	97.21		
4	SUM				100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00		

 BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668			BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER						PHASE: EB						
									PROJ. NO.1668			UNIT/ITM: 108			
MC:HEIDCO			HEAT AND MATERIAL BALANCE FOR SWS UNIT						SPEC. NO: 108-GP-E-411833			SH/OF: 3 / 8			
			REV.		0	1	2	B0							
1	Stream No.			06		07		08		09		10			
2	Stream Name			SOUR WATER TO FILTER COALESCER		PREHEATED SOUR WATER TO STRIPPER		SOUR WATER TO STRIPPER		ACID GAS FROM STRIPPER		COOLED ACID GAS TO REFLUX DRUM			
3															
4	Stream Description		Unit												
5	Vapor Mass Percent		wt%	0.00		0.00		0.09		100.00		35.78			
6	Temperature		°C	54		85		85		116		90			
7	Pressure		bar (g)	7.1		5.7		1.6		1.5		1.3			
8	Total Mass Flow		kg/h	99133.7		99133.7		99133.7		9613.1		9613.1			
9	Total Mol Flow		kmol/h	5456.4		5456.4		5456.4		477.8		477.8			
10	Total Heat Flow		MW	-423.61		-420.13		-420.13		-22.86		-26.54			
11	Total Molecular Weight		kg/kmol	18.17		18.17		18.17		20.12		20.12			
12	Total Flowing Density		kg/m³	956.0		939.2		735.6		1.6		5.1			
13															
14	Liquid Phase														
15	Mass Flow Rate		kg/h	99133.7		99133.7		99047.8				6173.4			
16	Molar Flow Rate		kmol/h	5456.4		5456.4		5453.8				333.2			
17	Flow Rate @ op. cond.		m³/h	103.7		105.5		105.4				6.9			
18	Standard Volume Flow Rate		m³/h	102.5		102.5		102.3				6.5			
19	Molecular Weight		kg/kmol	18.17		18.17		18.16				18.53			
20	Flowing Density		kg/m³	956.0		939.2		939.8				889.1			
21	Specific Gravity @ 15/15 °C		-	0.9685		0.9685		0.9690				0.9553			
22	Viscosity		cP	0.4585		0.2975		0.2986				0.2587			
23	Surface Tension		dyne/cm	45.93		36.44		42.96				53.15			
24	Mass Enthalpy		kJ/kg	-15383.4		-15257.0		-15268.2				-13480.3			
25	Mass Heat Capacity		kJ/(kg.°C)	3.9522		4.2138		4.2152				4.2898			
26	Thermal Conductivity		W/(m.K)	0.6138		0.5613		0.5722				0.5944			
27															
28	Vapor Phase														
29	Mass Flow Rate		kg/h					85.9		9613.1		3439.7			
30	Molar Flow Rate		kmol/h					2.6		477.8		144.6			
31	Flow Rate @ op. cond.		m³/h					29.4		6053.6		1860.8			
32	Molecular Weight		kg/kmol					32.99		20.12		23.79			
33	Flowing Density		kg/m³					2.9233		1.5880		1.8485			
34	Viscosity		cP					0.0142		0.0106		0.0113			
35	Compressibility Factor		-					0.9830		0.9833		0.9860			
36	CP/Cv Ratio		-					1.2474		1.3279		1.3175			
37	Mass Enthalpy		kJ/kg					-2344.8		-8560.5		-3584.0			
38	Mass Heat Capacity		kJ/(kg.°C)					1.3505		1.7756		1.5264			
39	Thermal Conductivity		W/(m.K)					0.0220		0.0273		0.0259			
40															
41	Stream Composition			mol %	wt %	mol %	wt %	mol %	wt %	mol %	wt %	mol %	wt %		
42	N2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
43	H2			0.00	0.00	0.00	0.00	0.00	0.00	0.02	0.00	0.02	0.00		
44	C2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
45	C3			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
46	C4			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
47	C5+			0.00	0.02	0.00	0.02	0.00	0.02	0.05	0.21	0.05	0.21		
48	CO2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
49	H2S			0.99	1.87	0.99	1.87	0.99	1.87	14.02	23.75	14.02	23.75		
50	NH3			0.96	0.90	0.96	0.90	0.96	0.90	18.05	15.27	18.05	15.27		
3	Water			98.04	97.21	98.04	97.21	98.04	97.21	67.86	60.76	67.86	60.76		
4	SUM			100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00		

 BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668			BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER						PHASE: EB						
									PROJ. NO.1668			UNIT/ITM: 108			
MC:HEIDCO		 Research Institute of Petroleum Industry		HEAT AND MATERIAL BALANCE FOR SWS UNIT						SPEC. NO: 108-GP-E-411833			SH/OF: 4 / 8		
				REV.		0	1	2	B0						
1	Stream No.			11		12		13		14		15			
2	Stream Name			ACID GAS FROM REFLUX DRUM		ACID GAS TO HEADER		ACID GAS TO SRU		REFLUX TO PUMP		REFLUX FROM PUMP			
3															
4	Stream Description		Unit												
5	Vapor Mass Percent		wt%	100.00		100.00		100.00		0.00		0.00			
6	Temperature		°C	90		90		89		90		90			
7	Pressure		bar (g)	1.3		1.1		1.1		(Note 3)		6.0			
8	Total Mass Flow		kg/h	3439.7		3439.7		3456.9		6173.4		6173.4			
9	Total Mol Flow		kmol/h	144.6		144.6		145.1		333.2		333.2			
10	Total Heat Flow		MW	-3.43		-3.43		-3.44		-23.12		-23.11			
11	Total Molecular Weight		kg/kmol	23.79		23.79		23.82		18.53		18.53			
12	Total Flowing Density		kg/m³	1.8		1.7		1.7		889.1		888.9			
13															
14	Liquid Phase														
15	Mass Flow Rate		kg/h							6173.4		6173.4			
16	Molar Flow Rate		kmol/h							333.2		333.2			
17	Actual Volume Flow Rate		m³/h							6.9		6.9			
18	Standard Volume Flow Rate		m³/h							6.5		6.5			
19	Molecular Weight		kg/kmol							18.53		18.53			
20	Flowing Density		kg/m³							889.1		888.9			
21	Specific Gravity @ 15/15 °C		-							0.9553		0.9553			
22	Viscosity		cP							0.2587		0.2580			
23	Surface Tension		dyne/cm							53.15		53.11			
24	Mass Enthalpy		kJ/kg							-13480.3		-13479.0			
25	Mass Heat Capacity		kJ/(kg.°C)							4.2898		4.2892			
26	Thermal Conductivity		W/(m.K)							0.5944		0.5944			
27															
28	Vapor Phase														
29	Mass Flow Rate		kg/h	3439.7		3439.7		3456.9							
30	Molar Flow Rate		kmol/h	144.6		144.6		145.2							
31	Flow Rate @ op. cond.		m³/h	1860.6		2037.6		2044.5							
32	Molecular Weight		kg/kmol	23.79		23.79		23.82							
33	Flowing Density		kg/m³	1.8486		1.6881		1.6908							
34	Viscosity		cP	0.0142		0.0142		0.0142							
35	Compressibility Factor		-	0.9860		0.9872		0.9872							
36	CP/Cv Ratio		-	1.3160		1.3148		1.3137							
37	Mass Enthalpy		kJ/kg	-3594.0		-3594.0		-3584.8							
38	Mass Heat Capacity		kJ/(kg.°C)	1.5304		1.5284		1.5307							
39	Thermal Conductivity		W/(m.K)	0.0247		0.0247		0.0248							
40															
41	Stream Composition			mol %	wt %	mol %	wt %	mol %	wt %	mol %	wt %	mol %	wt %		
42	N2			0.00	0.00	0.00	0.00	0.00	0.01	0.00	0.00	0.00	0.00		
43	H2			0.07	0.01	0.07	0.01	0.25	0.02	0.00	0.00	0.00	0.00		
44	C2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
45	C3			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
46	C4			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
47	C5+			0.16	0.59	0.16	0.59	0.24	0.88	0.00	0.00	0.00	0.00		
48	CO2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
49	H2S			37.55	53.78	37.55	53.78	37.51	53.67	3.82	7.02	3.82	7.02		
50	NH3			36.13	25.86	36.13	25.86	35.99	25.73	10.20	9.37	10.20	9.37		
3	Water			26.09	19.75	26.09	19.75	26.00	19.67	85.98	83.61	85.98	83.61		
4	SUM			100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00		

 BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668			BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER						PHASE: EB						
									PROJ. NO.1668			UNIT/ITM: 108			
MC:HEIDCO		 Research Institute of Petroleum Industry		HEAT AND MATERIAL BALANCE FOR SWS UNIT						SPEC. NO: 108-GP-E-411833			SH/OF: 5 / 8		
				REV.		0	1	2	B0						
1	Stream No.			16		17		18		19		20			
2	Stream Name			REFLUX TO STRIPPER		STRIPPER TO REBOILER		REBOILER VAPORS TO STRIPPER		STRIPPED WATER TO STRIPPER BOTTOM		STRIPPED WATER FROM STRIPPER			
3															
4	Stream Description		Unit												
5	Vapor Mass Percent		wt%	0.00		0.00		100.00		0.00		0.00			
6	Temperature		°C	90		133		133		133		133			
7	Pressure		bar (g)	5.1		2.1		2.0		2.0		2.2			
8	Total Mass Flow		kg/h	6173.4		112520.6		16826.6		95694.0		95694.0			
9	Total Mol Flow		kmol/h	333.2		6245.9		934.0		5311.9		5311.9			
10	Total Heat Flow		MW	-23.11		-481.78		-61.83		-409.74		-409.74			
11	Total Molecular Weight		kg/kmol	18.53		18.02		18.02		18.02		18.02			
12	Total Flowing Density		kg/m³	888.8		919.1		1.6		919.1		919.1			
13															
14	Liquid Phase														
15	Mass Flow Rate		kg/h	6173.4		112520.6				95694.0		95694.0			
16	Molar Flow Rate		kmol/h	333.2		6245.9				5311.9		5311.9			
17	Actual Volume Flow Rate		m³/h	6.9		122.4				104.1		104.1			
18	Standard Volume Flow Rate		m³/h	6.5		110.9				94.3		94.3			
19	Molecular Weight		kg/kmol	18.53		18.02				18.02		18.02			
20	Flowing Density		kg/m³	888.8		919.1				919.1		919.1			
21	Specific Gravity @ 15/15 °C		-	0.9553		1.0157				1.0157		1.0157			
22	Viscosity		cP	0.2579		0.2056				0.2056		0.2056			
23	Surface Tension		dyne/cm	53.11		52.12				52.12		52.12			
24	Mass Enthalpy		kJ/kg	-13479.0		-15414.2				-15414.4		-15414.4			
25	Mass Heat Capacity		kJ/(kg.°C)	4.2895		4.4997				4.4998		4.4998			
26	Thermal Conductivity		W/(m.K)	0.5944		0.6879				0.6879		0.6879			
27															
28	Vapor Phase														
29	Mass Flow Rate		kg/h					16826.6							
30	Molar Flow Rate		kmol/h					934.0							
31	Flow Rate @ op. cond.		m³/h					10398.3							
32	Molecular Weight		kg/kmol					18.02							
33	Flowing Density		kg/m³					1.6182							
34	Viscosity		cP					0.0133							
35	Compressibility Factor		-					0.9796							
36	CP/Cv Ratio		-					1.3408							
37	Mass Enthalpy		kJ/kg					-13227.8							
38	Mass Heat Capacity		kJ/(kg.°C)					1.9456							
39	Thermal Conductivity		W/(m.K)					0.0272							
40															
41	Stream Composition			mol %	wt %	mol %	wt %	mol %	wt %	mol %	wt %	mol %	wt %		
42	N2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
43	H2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
44	C2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
45	C3			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
46	C4			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
47	C5+			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
48	CO2			0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00		
49	H2S			3.82	7.02	0.00	0.00	0.00	0.00	0.00	< 7 ppmw	0.00	< 7 ppmw		
50	NH3			10.20	9.37	0.00	0.00	0.01	0.01	0.00	< 23 ppmw	0.00	< 23 ppmw		
3	Water			85.98	83.61	100.00	100.00	99.99	99.99	100.00	100.00	100.00	100.00		
4	SUM			100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00	100.00		

[illegible]

 شرکت پالایش نفت بندرعباس BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668			BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER				PHASE: EB						
MC:HEIDCO			 Research Institute of Petroleum Industry		HEAT AND MATERIAL BALANCE FOR SWS UNIT				SPEC. NO: 108-GP-E-411833		SH/OF: 7 / 8		
REV.		0		1		2		B0					
1	Stream No.			26		27		28		29			
2	Stream Name			STRIPPED WATER TO PROCESS UNITS		STRIPPED WATER TO WWT UNIT		STRIPPED WATER TO WWT UNIT		LS FROM B.L.			
3													
4	Stream Description		Unit										
5	Vapor Mass Percent		wt%	0.00		0.00		0.00		100.00			
6	Temperature		°C	45		45		45		210			
7	Pressure		bar (g)	6.3		6.3		5.6		4.1			
8	Total Mass Flow		kg/h	45777.0		49917.0		49917.0		16318.7			
9	Total Mol Flow		kmol/h	2541.0		2770.8		2770.8		905.8			
10	Total Heat Flow		MW	-200.92		-219.09		-219.09		-59.15			
11	Total Molecular Weight		kg/kmol	18.02		18.02		18.02		18.02			
12	Total Flowing Density		kg/m³	992.3		992.3		992.3		2.4			
13													
14	Liquid Phase												
15	Mass Flow Rate		kg/h	45777.0		49917.0		49917.0					
16	Molar Flow Rate		kmol/h	2541.0		2770.8		2770.8					
17	Actual Volume Flow Rate		m³/h	46.1		50.3		50.3					
18	Standard Volume Flow Rate		m³/h	45.1		49.2		49.2					
19	Molecular Weight		kg/kmol	18.02		18.02		18.02					
20	Flowing Density		kg/m³	992.3		992.3		992.3					
21	Specific Gravity @ 15/15 °C		-	1.0157		1.0157		1.0157					
22	Viscosity		cP	0.5937		0.5937		0.5935					
23	Surface Tension		dyne/cm	68.61		68.61		68.61					
24	Mass Enthalpy		kJ/kg	-15800.7		-15800.7		-15800.7					
25	Mass Heat Capacity		kJ/(kg.°C)	4.3173		4.3173		4.3174					
26	Thermal Conductivity		W/(m.K)	0.6376		0.6376		0.6376					
27													
28	Vapor Phase												
29	Mass Flow Rate		kg/h							16318.7			
30	Molar Flow Rate		kmol/h							905.8			
31	Flow Rate @ op. cond.		m³/h							6939.7			
32	Molecular Weight		kg/kmol							18.02			
33	Flowing Density		kg/m³							2.3515			
34	Viscosity		cP							0.0164			
35	Compressibility Factor		-							0.9751			
36	CP/Cv Ratio		-							1.3396			
37	Mass Enthalpy		kJ/kg							-13048.8			
38	Mass Heat Capacity		kJ/(kg.°C)							2.1461			
39	Thermal Conductivity		W/(m.K)							0.0348			
40													
41	Stream Composition			mol %		wt %		mol %		wt %			
42	N2			0.00		0.00		0.00		0.00			
43	H2			0.00		0.00		0.00		0.00			
44	C2			0.00		0.00		0.00		0.00			
45	C3			0.00		0.00		0.00		0.00			
46	C4			0.00		0.00		0.00		0.00			
47	C5+			0.00		0.00		0.00		0.00			
48	CO2			0.00		0.00		0.00		0.00			
49	H2S			0.00		< 7 ppmw		0.00		< 7 ppmw			
50	NH3			0.00		< 23 ppmw		0.00		< 23 ppmw			
3	Water			100.00		100.00		100.00		100.00			
4	SUM			100.00		100.00		100.00		100.00			

 BANDAR ABBAS OIL REFINING COMPANY شماره پروژه: 1668		BANDAR ABBAS OIL REFINERY HEAVY PRODUCTS QUALITY UPGRADING PROJECT BASED ON USING DELAYED COKER		PHASE: EB									
				PROJ. NO.1668				UNIT/ITM: 108					
MC:HEIDCO 		 Research Institute of Petroleum Industry		HEAT AND MATERIAL BALANCE FOR SWS UNIT		SPEC. NO: 108-GP-E-411833				SH/OF: 8 / 8			
						REV.	0	1	2	B0			
GENERAL NOTES: 1 - NA: NOT APPLICABLE NOTES: 1- This stream is intermittent flow, and is averagely 113.8 kg/hr (1.4 kmol/h, 0.2 m³/h). Standard Volume Flow Rate: 0.2 m³/h Total Heat Flow: -0.07 MW 2 - Stripped water specifications are as follows: Maximum H2S content is 7 ppmw Maximum NH3 content is 23 ppmw 3 - Pressure is in accordance with Hydraulic Calculation.													